

Notes

An Unusually Stable Supported Bis(cyclopentadienyl)titanium Dichloride-Trialkylaluminum Catalyst System for Ethylene Polymerization¹

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Introduction

A homogeneous bis(cyclopentadienyl)titanium(IV) dichloride-dialkylaluminum chloride catalyst system was first shown by Breslow and Newburg to polymerize ethylene.² Kinetic studies by Chien established that the active tetravalent titanium species undergo bimolecular decay to inactive trivalent species.³ Analogous zirconium compounds show no polymerization activity.⁴ The basic kinetic and mechanistic features of soluble metallocene catalysts have been reviewed.⁵ The distinguishing feature of this catalyst system is rapid decay as well as loss of catalyst activity within minutes of the start of polymerization and at temperatures higher than 30 °C.

One of the early attempts to heterogenize a soluble catalyst was due to Slotfeldt-Ellingsen and co-workers.⁶ Cp_2TiCl_2 was supported on silica gel and used to polymerize ethylene using $\text{Et}_n\text{AlCl}_{3-n}$ as cocatalyst. The specific catalyst activity was found to be comparable for both homogeneous and supported catalysts. More recently, Soga and co-workers have studied supported ethylenebis-(tetrahydroindenyl)zirconium(IV) dichloride for the isospecific polymerization of propylene.⁷ Al_2O_3 , MgCl_2 , and SiO_2 pretreated with methylaluminoxane (MAO) were used as supports and trialkylaluminum as cocatalyst. Al_2O_3 and MgCl_2 gave low molecular weight polymers with broad polydispersity.⁸ On the contrary, SiO_2 pretreated with MAO gave narrow polydispersities and lower catalyst activity. MAO-pretreated-silica supported metallocene catalyst has been shown to polymerize propylene with no change of stereospecificity.⁹ All the above catalysts were prepared by physical mixing of the support with the zirconium compound in a diluent such as toluene.

We now report for the first time a simple synthesis of a MgCl_2 supported Cp_2TiCl_2 catalyst which shows significant activity for ethylene polymerization in the presence of trialkylaluminum and a kinetic behavior distinctly different from that of an unsupported metallocene catalyst.¹⁰

Experimental Section

Materials. Grignard-grade Mg turnings (Loba Chemical, India), bis(cyclopentadienyl)titanium(IV) dichloride (Cp_2TiCl_2 ; Aldrich), triisobutylaluminum (TIBAL), and diethylaluminum chloride (DEAC; Schering A. G., Germany) were used as received. 1,2-Dichloroethane (SD Fine Chemicals, Bombay) was distilled over CaH_2 and stored over 3-Å molecular sieves. Tetrahydrofuran (THF), hexane, and xylene were purified by distilling over sodium. Polymer-grade ethylene was obtained from the Gas Cracker Complex of Indian Petrochemicals Corp., Ltd., at Nagothane,

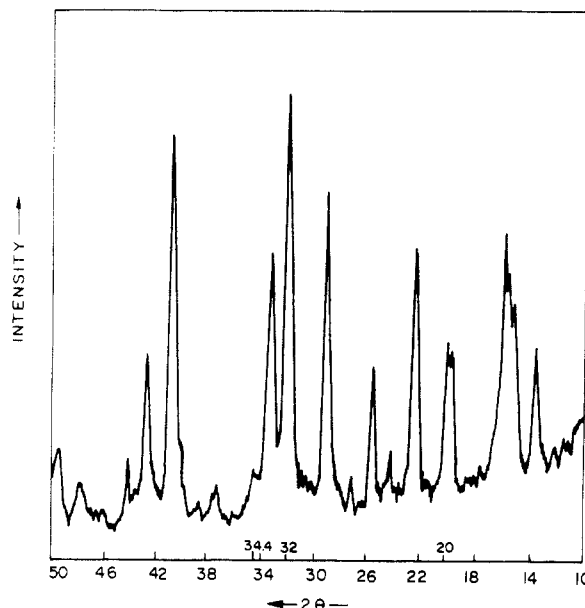


Figure 1. Powder XRD pattern of Cp_2TiCl_2 supported on MgCl_2 . India. It had a moisture content of <4 ppm (Shaw Model SHA-TR moisture analyzer) and an oxygen content of <3 ppm (Braun oxygen analyzer). All manipulations involving air-sensitive compounds were performed inside a Labconco Model 50004 inert-atmosphere glovebox continuously purged with high-purity N_2 (<5 ppm moisture) generated using a N_2 generator (Spantech Model NG 300-1, England) or under a positive pressure of high-purity N_2 using standard bench-top inert-atmosphere techniques.

Catalyst Synthesis. Two supported Cp_2TiCl_2 catalysts having 1.8 and 3.3% by weight of titanium were used in this study (catalysts A and B, respectively). A typical procedure for the synthesis of catalyst is as follows.

A three-neck round-bottomed flask equipped with a magnetic stirring bar, N_2 inlet, addition funnel, and reflux condenser was flame dried and cooled under a N_2 atmosphere. Iodine (5 mg) activated magnesium turnings (0.4 g) were placed in the flask, and THF (30 mL) was added. The slurry was stirred for 30 min at 40 °C. A mixture of 1,2-dichloroethane and THF (1:1) (40 mL) was transferred into the addition funnel using a cannula and added dropwise at 40–50 °C. It was observed that all the Mg turnings slowly dissolved in THF with the formation of a clear solution. Steady evolution of ethylene gas was observed, indicating decomposition of the intermediate β -chloroethylmagnesium chloride to a complex of MgCl_2 and THF and its dissolution in THF. The clear solution was further diluted by addition of 20 mL of THF, separated from traces of unreacted magnesium, and transferred into another flame-dried three-neck flask equipped with a magnetic stirring bar, N_2 inlet, addition funnel, and septum.

Cp_2TiCl_2 (3.36 mmol) was dissolved in THF in a flame-dried round-bottomed flask. The clear dark-red solution was then transferred into an addition funnel using a cannula. The Cp_2TiCl_2 -THF solution was added dropwise into the MgCl_2 -THF solution. It was observed that no separation of layers or any solid material occurred. This red solution was then added slowly to 300 mL of dry hexane. A solid precipitate having a whitish pink color separated out. The solid was dried under vacuum at 40 °C. The dried solid was transferred into vials and stored in the glovebox. Yield: 4.2 g. Anal. Calcd: Mg, 10.8; Ti, 3.3; Cl, 35.9.

Polymerization. Ethylene polymerization was performed in a stirred glass reactor at 1 atm in xylene using about 100–120 mg

Table I. Ethylene Polymerization with Unsupported and Supported Catalyst^a

sample no.	catalyst	cocatalyst	time (min)	PE (g)	convn (%)	R_p ($M s^{-1}$)	activity (kg of PE/mol of Ti)	$[\eta]^c$ (dL/g)
1	Cp_2TiCl_2	TIBAL	60			no polymerization activity		
2 ^b	Cp_2TiCl_2	DEAC	10	0.30	100	1.37	0.9	0.3
3	catalyst B	TIBAL	60	0.48	100	0.39	2.4	3.5
4	catalyst B	DEAC	60	0.61	100	1.69	6.4	0.9

^a All polymerizations were performed at 40 °C in xylene medium at Al/Ti = 50 at a total pressure of 1 atm. ^b Ethylene absorption ceased after a lapse of 10 min. ^c Intrinsic viscosities were determined in *o*-dichlorobenzene at 135 °C.

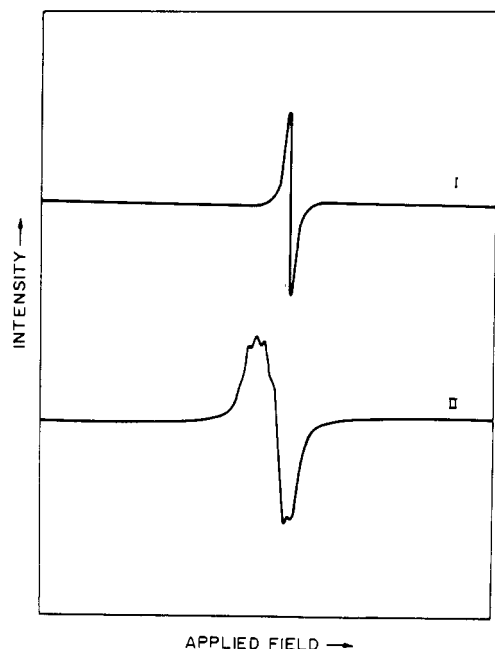


Figure 2. ESR spectra of (I) Cp_2TiCl_2 -TIBAL and (II) $Cp_2TiCl_2/MgCl_2$ -TIBAL in xylene at 25 °C; $[Ti] = 1.25 \times 10^{-4}$ mol, Al/Ti = 50.

Table II. Effect of the Al/Ti Ratio on Ethylene Polymerization with the Mg-Ti/TIBAL Catalyst System^a

sample no.	Ti (wt %)	Al/Ti wt ratio	convn (%)	R_p ($M s^{-1}$)	activity (kg of PE/mol of Ti)	$[\eta]^b$ (dL/g)
1	3.3	50	95	0.39	2.5	2.6
2	3.3	100	97	0.51	2.5	3.6
3	3.3	200	99	0.68	2.0	4.7
4	1.8	50	99	0.18	0.8	2.2
5	1.8	100	98	0.48	1.0	3.4
6	1.8	200	98	0.61	2.0	4.0

^a All polymerizations were performed at 40 °C for 60 min in xylene at a total pressure of 1 atm. ^b Intrinsic viscosities were determined in *o*-dichlorobenzene at 135 °C.

of solid catalyst in conjunction with cocatalyst. The reactor assembly and manner of conducting polymerization has been described elsewhere.¹¹

Analysis. Titanium estimation was performed using a Hitachi Model 220 UV-visible spectrophotometer. Mg and Cl estimations were performed by EDTA and argentometric titrations. ESR spectra were run on a Bruker Model ER-200D ESR spectrometer at room temperature (9.72 GHz). Powder XRD was recorded on a Philips PW 1730 spectrometer using nickel-filtered $Cu K_\alpha$ radiation. FT-IR spectra were run on a Perkin-Elmer 16PC FT-IR in Nujol mull using NaCl cells (1600–400 cm^{-1}). Viscosities of the polymer samples were determined using an Ubbelohde viscometer in *o*-dichlorobenzene as solvent at 135 °C.

Results and Discussion

Two heterogeneous magnesium-titanium catalysts, having 1.8 and 3.3% of titanium, synthesized in the present

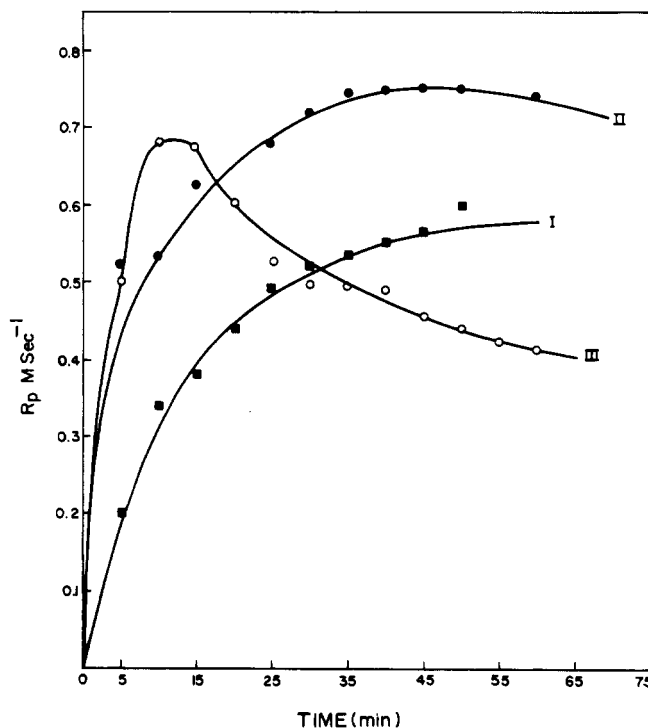


Figure 3. Plot of rate of polymerization versus time for the $Cp_2TiCl_2/MgCl_2$ -TIBAL catalyst system in xylene at 40 °C; $[Ti] = 1.84 \times 10^{-4}$ mol; (I) Al/Ti = 50, (II) Al/Ti = 100, and (III) Al/Ti = 200.

study, were observed to have the empirical formulae $MgTi_{0.05}Cl_{2.0}Cp_{0.1}(THF)_{0.5}$ and $MgTi_{0.15}Cl_{2.09}Cp_{0.3}(THF)_{1.2}$ as calculated from the corresponding elemental analysis. The FT-IR spectrum of the solid catalyst showed distinct bands at 1460 and 820 cm^{-1} characteristic of C–C stretching and C–H deformation bands of the cyclopentadienyl ring.¹² It also showed at 1036 and 888 cm^{-1} characteristic vibration bands of THF bound to the solid surface.¹³ The powder XRD pattern of the Mg-Ti catalyst showed the absence of a strong reflection at $2\theta = 34.4^\circ$ and a reduction in the intensity of a reflection at $2\theta = 20^\circ$ both of which were originally present in Cp_2TiCl_2 . A new reflection at $2\theta = 32^\circ$ appeared in the Mg-Ti catalyst (Figure 1) corresponding to that of the $MgCl_2$ -THF complex. $MgCl_2$ -THF is formed by the in situ Grignard decomposition of the intermediate β -chloroethylmagnesium chloride. Upon reduction with TIBAL, the Mg-Ti catalyst showed a splitting in the spectrum in contrast to a sharp single peak at $g = 1.98$ for Cp_2TiCl_2 (Figure 2). This indicates that the metallocene is heterogenized on the support.⁶

In the presence of TIBAL, Cp_2TiCl_2 is inactive toward polymerization of ethylene. Substitution of TIBAL with DEAC causes initiation of polymerization; however, the catalyst system is short lived and rapidly decays. Ethylene absorption ceases within 10 min of mixing the catalyst components. In contrast, Cp_2TiCl_2 supported on $MgCl_2$ shows a significant polymerization activity even with TIBAL and a 3-fold increase in activity with DEAC (Table

Table III. Effect of Temperature on Ethylene Polymerization with the Mg-Ti/TIBAL Catalyst System^a

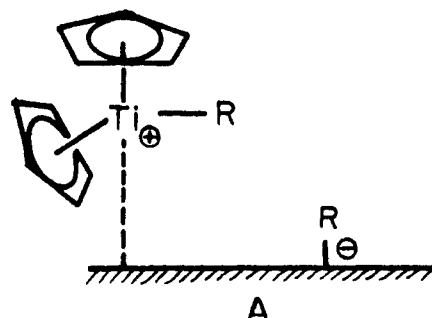
sample no.	Ti (wt %)	temp (°C)	PE (g)	convn (%)	R_p ($M s^{-1}$)	activity (kg of PE/mol of Ti)	$[\eta]^b$ (dL/g)
1	3.3	40	0.25	93.6	0.51	2.5	3.52
2	3.3	60	0.16	33.3	0.76	1.2	1.47
3	3.3	70	0.08	22.2	1.29	0.7	0.79
4	1.8	40	0.18	99.0	0.18	0.7	3.42
5	1.8	60	0.08	60.0	0.19	0.5	2.20
6	1.8	70	0.07	50.0	0.33	0.4	1.40

^a All polymerizations were performed at Al/Ti = 100 in xylene for 60 min at a total pressure of 1 atm. ^b Intrinsic viscosities were determined in *o*-dichlorobenzene at 135 °C.

I). More interestingly, the catalyst system shows a steady-state kinetic behavior. The increase in molecular weight upon heterogenization shows that the propagation is faster or that the chain-transfer process is slowed down relative to the soluble catalyst or that different chain-transfer processes are operating.

The effect of the Al/Ti weight ratio on the polymerization behavior was studied with the two Mg-Ti catalysts. The results are shown in Table II (Figure 3). The catalyst activity increased with increasing Al/Ti ratio for a catalyst containing a lower titanium content. The polymer molecular weights showed a steady increase with increasing Al/Ti ratio, indicating the organoaluminum compound did not contribute significantly to the chain-transfer process. Conversion and molecular weight decreased with increasing reaction temperature (Table III). The decrease was more severe in the case of the catalyst containing a higher titanium content.

These results suggest that $MgCl_2$ confers unusual stability to an otherwise unstable active polymerization center. Dramatic enhancement in catalytic activity has been reported for $Cp_2Th(CH_3)_2/MgCl_2$ for propylene hydrogenation.¹⁴ On the basis of a ¹³C CP-MAS NMR study of $Cp_2Th(CH_3)_2/MgCl_2$, it was concluded that the active center was a "cation-like" complex formed by the transfer of methide anion from the actinide center to the Lewis acidic sites on the surface of $MgCl_2$.¹⁵ A similar mechanism can be invoked to explain the unusual activity as well as stability of the $Cp_2TiCl_2/MgCl_2$ -trialkylaluminum catalyst system for ethylene polymerization. Although we have no experimental evidence at the present time, we presume that the active site is a cation-like complex of Cp_2TiR^+ adsorbed on $MgCl_2$ (A), where the reactive sites are isolated on the support, thereby stabilizing the coordinatively unsaturated monomeric titanium species. Matrix isolation of catalytically active sites in



the case of Cp_2TiCl_2 chemically anchored to rigid polymeric support has been shown to be responsible for higher rates of olefin hydrogenation observed with supported Cp_2TiCl_2 compared to Cp_2TiCl_2 in solution.¹⁶

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